

Adjoint-based Shape Optimization for Turbulent Convective Heat Transfer with a Hybrid RANS-DNS Approach

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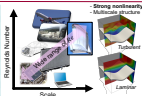


Heat Exchanger Design

Dilemma: Strong similarity between Heat transfer & Drag

⇒ **Origin of dissimilarity**
Momentum ⇒ Divergence-free vector
Energy ⇒ Conservative Scalar

e.g. Optimal control theory can achieve complete dissimilar control, Yamamoto et al., J. Fluid Mech. (2013)



Shape optimization algorithm for turbulent convective heat transfer is needed.

Shape optimization strategy for turbulent flow

	1) Steady approach	2) Unsteady approach
On/Off	RANS Simulation (steady)	DNS/LES (unsteady)
Pros/Cons	- Accuracy of turbulence model	- High cost - Highly accurate prediction
Approach	Steady adjoint simulation	Unsteady adjoint simulation Invalid due to the strong nonlinearity
Objective	Performance is not guaranteed due to low accuracy of forward analysis.	To be established ⇒ Present study, 1)
	3) DNS-RANS Hybrid Approach "RANS-based adjoint analysis" + "Turbulent statistics from DNS"	

Objective:
Development of adjoint-based shape optimization algorithm for turbulent convective heat transfer with DNS-based Eddy Viscosity & Diffusivity

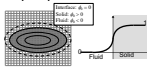
Optimization Algorithm

Target: Wavy Fin

Shape Expression



Uniformly heated fluid is cooled by the channel walls and wavy fin



Level-set Function, ϕ_b ⇒ Shape indicator, ϕ
Optimal shape ⇔ Optimal distribution of ϕ

Governing equations & Numerical set-up

$$\begin{cases} \frac{\partial \mathbf{u}}{\partial t} = -\nabla(\mathbf{u}\mathbf{u}) + \frac{1}{Re} \nabla^2 \mathbf{u} - \nabla p - \eta \phi \mathbf{u} \\ \frac{\partial \theta}{\partial t} = -\nabla(\theta \mathbf{u}) + \frac{1}{Pe} \nabla^2 \theta + Q - \eta \phi \theta \\ \nabla \cdot \mathbf{u} = 0 \end{cases}$$

Impose no-slip & isothermal conditions on fin by **Volume Penalization Method**
e.g. Peskin C. S., J. Comput. Phys. 10 (1972) 37

$Re = \frac{u_c \delta}{\nu} = 200$
 $Pe = Re Pr = 200$
 δ : channel-half width
 ν : kinematic viscosity
 u_c : friction velocity

[Boundary conditions]
Streamwise, z : Periodic boundary
Spanwise, x : Periodic boundary
Wall-normal, y : $(u,v,w) = \theta = \theta = 0$

[Flow conditions]
Constant mean pressure gradient
Constant uniform heating of the fluid

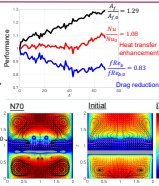
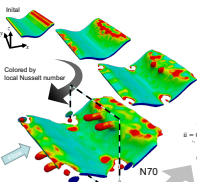
[Domain Size]
 $(L_x, L_y, L_z) = (20, 20, 20)$
[No. of grid points]
 $(N_x, N_y, N_z) = (120, 120, 120)$
[Scheme]
Spatial discret.: 2nd order FD
Time integration: RK3/CN2
Pressure coupling: SMAC

Cost Functional

"More heat transfer with less pressure drag"
⇒ "Maximizing the ratio of heat transfer to pressure drop. Analogy factor, A_f "

$$J = -A_f = -\frac{Nu}{f Re_b} = \frac{\text{Dimensionless heat transfer coefficient}}{\text{Dimensionless pumping power}}$$

Results & Discussion



Mechanism

Drag Reduction

- Flow rate increase by
- Cross sectional area increase
- Suppression of recirculation region

Heat transfer Enhancement

- Secondary flow enhancement by
- Holes on fin-crest near channel side-wall
- Streamwise protrusion at the channel-center region

Summary

- New adjoint-based shape optimization algorithm for convective turbulent heat transfer is proposed and validated with a wavy fin.
- The present algorithm uses turbulent statistics obtained by DNS for tuning of eddy viscosity and diffusion in RANS-based adjoint analysis.